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## Feed-forward Control of Thermal Power Plants Using Neural Networks

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**Abstract :** In thermal power plants, it is an important theme to improve the control performance of main steam pressure and temperature etc. during load up/down. This paper focuses on temperature control that is the most difficult problem due to the non-linearity and long dead times of power plants. Model Reference Adaptive Control (MRAC) is applicable to the feed-forward control of power plants, but there are some problems. The most serious problem is that persistently exciting (PE) condition is not satisfied, and so it is difficult to estimate plant parameters using the well-known recursive least squares method. It is proposed in this paper that Jacobians of the neural networks (NN) are applied to identify the above mentioned plant parameters and control law is obtained by two methods, that is, one is the method to use the Jacobians of the NN plant model which is obtained by off line forward model learning, the other is the method to utilize the Hessian of the cost function. This method is evaluated by a detailed simulator that represents accurately the dynamics of power plants, and usefulness and effectiveness of the proposed method is proved.

**Keywords :** Control systems, Non-linear control, Thermal power plants, Neural networks

### 1. Introduction

This paper describes the application of neural networks to the feed-forward control to thermal power plants. In thermal power plants, not only feedback control, but also feed-forward control is necessary to keep main steam temperature, pressure etc. to the set values during load up/down. It is difficult to determine this feed-forward control signal in the complex system such as a thermal plant. We have studied the application of MRAC<sup>1)</sup> to the problem mentioned above. But in the process control where the process value changes slowly, it has become clear that PE condition is not satisfied, so it is difficult to estimate the plant parameters by recursive least squares method of MRAC. In place of MRAC, we consider in this paper the application of NN to the control of the thermal power plant. NN has been applied in many industrial fields such as, for example, pattern recognition, robotics etc., but only a few examples have been reported in the process control fields. Application of NN to the power system control involves many problems to be solved. The main problem is that frequent load up/down for training NN is not permissible, so it is difficult to train on line. Two off line NN training schemes can be employed in controller design, however they still have unsolved

problems :

(a) Generalized learning<sup>2)</sup>. An inverse NN model of the plant is trained and then used as a controller, which does not always give a well-trained good NN controller.

(b) Forward model learning. An inverse of a trained NN model of the plant is derived by a certain method and is employed as a controller, where the inversion is a relatively difficult task. Details of (a) and (b) will be discussed later.

In this paper we develop two methods to obtain the on line control law which are based on the off line forward model learning. One is the method to use the Jacobian of the NN plant model which is obtained by off line forward model learning, the other is the method to utilize the Hessian of the cost function. Temperature control of thermal power plants is discussed in the following sections, which is the most difficult theme for control because of non-linearity and long dead times.

We confirm that the proposed method is very effective by a detailed simulator that represents accurately the dynamics of plant.

The paper is organized as follows : Section 2 briefly describes the plant model. In Section 3, several existing NN control schemes are surveyed with an emphasis on their drawbacks in their application to power plants control. The proposed NN control scheme is described in detail in Sections 4-7. Section 8 gives simulation results of the proposed methods. Finally, Section 9 is devoted to discussions and conclusions.

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## 2. Plant model

The conventional controller configuration and plant model are described in this Section, which serves as a basis for the proposed NN controller. **Fig. 1** shows the outline of the conventional temperature control system. Fuel supply signal consists of the following three items.

(a) Statistic Feed-forward signal (SF) which corresponds to Mega Watt Demand (MWD).

(b) Proportional and Integral (PI) signal obtained by the feedback of the difference between set-point and measured temperature  $y(t)$ .

(c) Transient Feed-forward signal (TF) which compensates the control lag of the PI control.

The TF and PI parts are replaced with an NN based controller, whose output signal is denoted as Dynamic Feed-forward Control signal (DFC). Our objective in this paper is to determine the DFC of **Fig. 1** by an NN model. Approximating the plant by linearization, plant model is represented by (1),

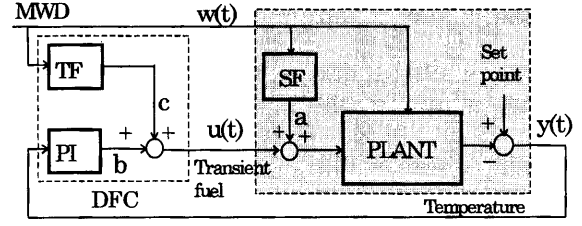
$$\begin{aligned} A(z^{-1})y(t) &= z^{-d}B(z^{-1})u(t), \\ A(z^{-1}) &= 1 + a_1z^{-1} + a_2z^{-2} + \dots + a_nz^{-n}, \\ B(z^{-1}) &= b_0 + b_1z^{-1} + b_2z^{-2} + \dots + b_mz^{-m}. \end{aligned} \quad (1)$$

Applying (1) to the temperature control of **Fig. 1**, the input variable, the output variable and the disturbance added to the input correspond to DFC ( $u(t)$ ), temperature ( $y(t)$ ) and MWD ( $w(t)$ ), respectively. So the plant is rewritten by (2),

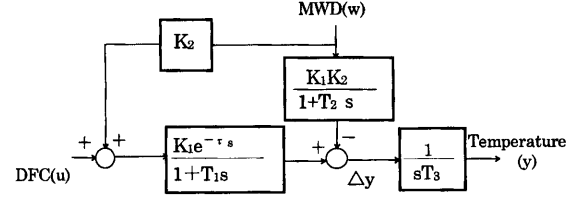
$$\begin{aligned} A(z^{-1})y(t) &= z^{-d}B(z^{-1})u(t) + C(z^{-1})w(t), \\ A(z^{-1}) &= 1 + a_1z^{-1} + a_2z^{-2} + \dots + a_nz^{-n}, \\ B(z^{-1}) &= b_0 + b_1z^{-1} + b_2z^{-2} + \dots + b_mz^{-m}, \\ C(z^{-1}) &= c_0 + c_1z^{-1} + c_2z^{-2} + \dots + c_kz^{-k}, \\ w(t) &: \text{disturbance} \cdots \text{MWD}, \\ u(t) &: \text{control law} \cdots \text{fuel (DFC=PI=TF)}, \\ y(t) &: \text{controlled object} \cdots \text{temperature}, \\ &\quad (\text{set-point} \cdots \text{measured temperature}) \\ d &: \text{dead time}. \end{aligned} \quad (2)$$

First it is necessary to determine the value of  $n$ ,  $m$ ,  $k$  in (2) before applying NN to the power plant. Response of temperature from fuel is approximately expressed by first order lag and dead time, and that from MWD by first order lag. So, the simplified model of the power plant is shown in **Fig. 2**. Therefore the relation between  $y(t)$ ,  $u(t)$  and  $w(t)$  is given by

$$y = \left( \frac{K_1 e^{-\tau s}}{1 + T_1 s} u - K_1 K_2 \left( \frac{1}{1 + T_2 s} - \frac{e^{-\tau s}}{1 + T_1 s} \right) w \right) \frac{1}{T_3 s}$$



**Fig. 1** Outline of main steam temperature control system



**Fig. 2** Simplified model

(3)

By the  $z$ -transformation of (3), the following difference equation is obtained :

$$(1 + a_1z^{-1} + a_2z^{-2} + a_3z^{-3})y(t) = z^{-d}(b_0 + b_1z^{-1})u(t) + (c_0 + c_1z^{-1} + c_2z^{-2})w(t). \quad (4)$$

Applying Diophantine equation ( $1 = A(z^{-1})S(z^{-1}) + z^{-d}R(z^{-1})$ ) to (4), the following equation is obtained :

$$\begin{aligned} y(t+d) &= \{A(z^{-1})S(z^{-1}) + z^{-d}R(z^{-1})\}y(t+d) \\ &= R(z^{-1})y(t) + B(z^{-1})S(z^{-1})u(t) \\ &\quad + C(z^{-1})S(z^{-1})w(t+d). \end{aligned} \quad (5)$$

The order of  $S$ ,  $R$ ,  $BS$ ,  $CS$  is  $d-1$ ,  $2$ ,  $2d-1$ , respectively, so  $R$ ,  $BS$  and  $CS$  are given by

$$R(z^{-1}) = a_0 + a_1z^{-1} + a_2z^{-2}, \quad (6)$$

$$B(z^{-1})S(z^{-1}) = b_0 + b_1z^{-1} + \dots + b_dz^{-d}, \quad (7)$$

$$C(z^{-1})S(z^{-1}) = c_0 + c_1z^{-1} + \dots + c_{2d-1}z^{-(2d-1)}. \quad (8)$$

## 3. Application of NN

An NN is a mean to describe the input/output relationship and the first step is to use an NN to identify the plant model (5). The plant model (5) should be represented by the Eq.(9) due to its non-linearity,

$$\begin{aligned} y(t+d) &= f[u(t), u(t-1), \dots, u(t-d), w(t+d), \\ &\quad w(t+d-1), \dots, w(t-d+1), \\ &\quad y(t), y(t-1), y(t-2)]. \end{aligned} \quad (9)$$

Therefore utilizing an NN to identify the plant model is to construct Eq.(9) by the NN. From now

on, time  $t$  is indicated by a suffix.

Some training and control methods have been already proposed, for example, feedback error learning (Fig. 3(a))<sup>3</sup>, special learning (Fig. 3(b))<sup>2</sup>, generalized learning (Fig. 3(c))<sup>2</sup>, forward model learning (Fig. 3(d)), and forward and inverse model learning (Fig. 3(e)). Feedback error learning and special learning can be executed only when the plant model is known. This paper is focused on the problem where the plant is unknown. In the following, the learning and control methods are summarized which are appropriate for the case where the plant model is difficult to make, and the problems with these existing methods will be clarified.

#### A. Generalized learning

The input to the NN is the plant output, and the desired output is the control signal, i.e., by this learning method an inverse model of the plant is obtained. In this case, learning corresponds to determination of the following non-linear function that is the inverse of (9).

$$u_t = g[u_{t-1}, u_{t-2}, \dots, u_{t-d}, W_{t+d}, W_{t+d-1}, \dots, W_{t-d+1}, y_{t+d}, y_t, y_{t-1}, y_{t-2}] \quad (10)$$

After training the non-linear function, it is used in the on line control. But in this case function  $g$  contains errors (inevitable in NN), and so  $u_t$  has some errors, where  $u_{t+1}$  is a function of  $u_t$ , in the same way  $u_{t+2}$  is a function of  $u_{t+1}$ , and so on. As the result, errors of control input  $u_t$  are accumulated. We have confirmed this by simulations.

#### B. Forward model learning

The input to the NN is the control signal, and the desired output is the plant output, i.e., this learning method corresponds to the creation of the forward model of the plant. Thus non-linear function (9) is obtained. Therefore control input  $u_t$  can be obtained by the inverse of NN. Although the learning error is smaller than that of generalized learning, it is difficult to obtain control input by inverting Eq.(9) because of its non-linearity.

#### C. Forward and inverse model learning

This learning method is shown in Fig. 3(e). In this case, the NN is trained by the deviation between the target value and output of the plant. In this case Jacobian of the plant is necessary, but it is impossible to know the Jacobian if the plant is unknown. But when the plant is replaced by the plant model trained by forward model learning, the NN controller can be trained by using Jacobian calculated by the plant model. But in this case the NN is trained through two stages by which the error is accumulated and so good control performance is not expected. We have also confirmed this by simulations.

#### D. Determination of control law from forward model

Since forward model learning provides NN with small errors, an effective procedure for inverting them will be very useful in designing NN based controllers. Iterative inverse method (IIM)<sup>5)</sup> was proposed for the calculation of control input from the forward model. The output of NN;  $y_{t+d}$  is decided by input  $y_t, \dots, u_t, \dots, W_{t+d}, \dots$  (sequential data of output, control input and disturbance) and weights  $W$ .  $W$  is decided by the forward model learning. Key point in IIM is to determine  $u_t$  by the same method as the determination of  $W$  with  $W$  being fixed. But this method has following three problems. i.e., iterative calculation is necessary, and we have to determine appropriate learning rate and iteration number which depend on the situations. There are some other methods as for the determination of control law from the forward model. e.g., simplex method, but it also has the same problems.

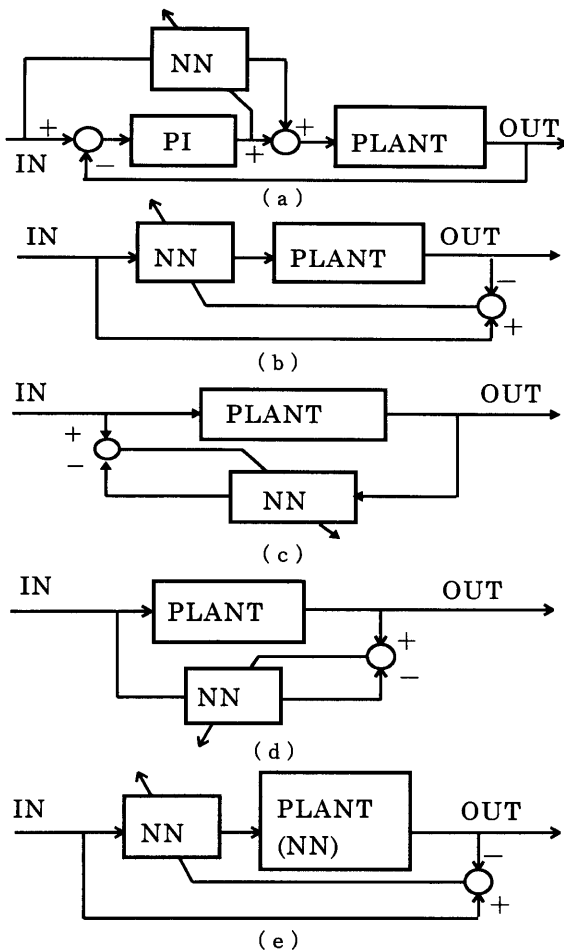


Fig. 3 Various training method

We propose two methods to solve these problems. The first one is the method named Jacobian method based on the assumption that the plant model is approximated linearly, and the second one called Hessian method uses Hessian in order to compute the control input.

#### 4. Learning of NN

The feature of training data measured from the thermal power plant is that it has a long duration and changes very slowly as compared with those from the servo systems such as robots. (refer to **Fig. 12**). We have to choose appropriate method for NN learning. These are various alternatives concerning the learning of NN. (a) Structure of neural network: Layered network with external memory, Layered network with first order lag, Recurrent network. (b) Learning algorithm: BP (Back Propagation), BPTT (Back Propagation Trough Time), RTRL<sup>6)</sup> (Real Time Recurrent Learning), RS<sup>7)</sup> (Random Search). (c) Input method: Random input, Sequential input. (d) Updating timing of the weights: updating after presentation of all the data (1 cycle), updating per each data presentation. We studied what combination of them is appropriate for our purpose. Various combinations are evaluated by simulations. Simulation results show that the combination of (a) layered networks with external memory, (b) BP, (c) random input and (d) updating per each data presentation is the best.

We used the off line forward model learning to model the power plant. **Fig. 4** shows the configuration of NN.

#### 5. Iterative inverse method

The IIM proposed by A. Linden et. al is summar-

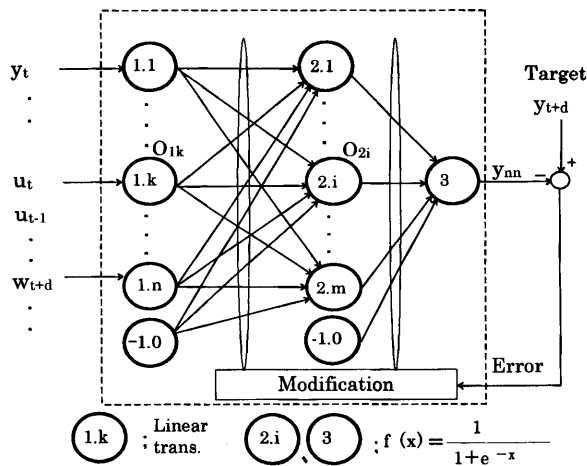


Fig. 4 Configuration of neural network

ized. **Fig. 5(a)** shows the forward model learning. Plant model is shown by  $y_{t+d} = f(y_t, y_{t-1}, \dots, u_t, u_{t-1}, \dots, w_{t+d}, w_{t+d-1}, \dots, W)$ . Inputs of NN are  $y_t, \dots, u_t, \dots, w_{t+d}, \dots$ , and NN output  $y_{nn}$  is compared to the supervised output  $y_{t+d}$ , and weights  $W$  is adjusted to minimize the difference between them as follows,

$$W^{(n)} = W^{(n-1)} - \eta' \cdot \frac{\partial (y_{t+d} - y_{nn})^2}{\partial W}, \quad (11)$$

where

$\eta'$ : learning rate of  $W$ .

**Fig. 5(b)** shows the principle of IIM,  $u_t$  can be calculated with  $W$  being fixed in almost the same way as the determination of  $W$ . Although  $W$  is trained off line in order to model the power plant,  $u_t$  is calculated on line to control the plant. The method of calculating  $u_t$  in **Fig. 5(b)** is as follows.

The cost function is defined by Eq.(12),

$$J = \frac{1}{2} ((d_{t+d} - y_{t+d})^2 + \rho \cdot u_t^2), \quad (12)$$

where

$\rho$ : Trade off coefficient between control accuracy and control energy. Inverse calculation of  $u_t$  is performed as follows in the same way as the adjusting of  $W$ ,

$$\begin{aligned} u_t^{(n)} &= u_t^{(n-1)} - \eta \cdot \frac{\partial J}{\partial u_t}, \\ &= u_t^{(n-1)} - \eta \cdot \left( (y_{t+d} - d_{t+d}) \cdot \frac{\partial y_{t+d}}{\partial u_t} + \rho \cdot u_t^{(n-1)} \right), \end{aligned} \quad (13)$$

where

$\eta$ : Learning rate of  $u_t$ .

Derivative  $\partial y_{t+d} / \partial u_t$  in Eq.(13) is calculated as follows for our NN depicted in **Fig. 4**,

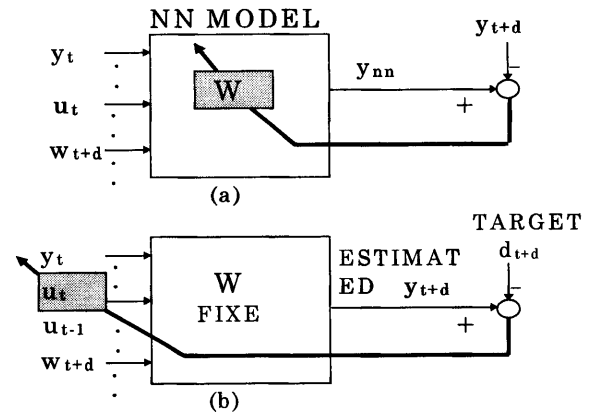


Fig. 5 Iterative inverse method

$$\begin{aligned}
\frac{\partial y_{t+d}}{\partial u_t} &= \sum_i \frac{\partial y_{t+d}}{\partial O_{2i}} \cdot \frac{\partial O_{2i}}{\partial u_t}, \\
&= \sum_i \{f'(\text{net}_3) \cdot W_i \cdot f'(\text{net}_{2i}) \cdot W_{ik}\}, \\
&= f'(\text{net}_3) \cdot \sum_i W_i \cdot f'(\text{net}_{2i}) \cdot W_{ik}, \\
\text{net}_{2i} &= \sum_k O_{1k} \cdot W_{ik}, \quad \text{net}_3 = \sum_i O_{2i} \cdot W_i.
\end{aligned} \tag{14}$$

But, iterative equation (13) has the following essential problems when it is used on line.

(a) Iterative calculation is to be finished before measuring the new data.

(b) Determination of appropriate learning rate  $\eta$  is necessary.

(c) Determination of iteration number is needed.

When weight  $W$  is calculated off line according to Eq.(11) in order to model the plant, then trial-and-error search for good learning rate and iteration number is permissible. But calculation of  $u_t$  is executed on line, so the time expenditure due to the iterative calculation mentioned above is not preferable, especially the above trial-and-error process is not permissible.

## 6. Jacobian method

In this and the following sections, two new methods for calculating control input  $u_t$  on line are presented in order to overcome those problems in the iterative inverse method mentioned in the previous section. The problems will be resolved if the inversion of the plant model can be performed either non-iteratively or with a fewer number of iterations. The first one is the Jacobian method that enables non-iterative inversion based on the concept that the linearized parameters (6)–(8) are equal to the Jacobian of the NN obtained by the forward model learning. The other one is the Hessian method whose feature is the high speed of the calculation of  $u_t$  by use of the second order derivative.

Recall that the linearized plant was represented by Eq.(5)–(8). Because of linearity of the equations, inversion of Eq.(5) can be easily performed, i.e. the equation is readily solved for  $u_t$ . Therefore control input  $u_t$  that minimizes the cost function Eq.(12) can be derived without any iterative calculation. However the parameters  $a_i$ ,  $b_j$ ,  $c_k$  in Eq.(6)–(8) depend on the operating point, and their on line estimation is required. Here, it is important to point out that  $a_i$  is equivalent to  $\partial y_{t+d}/\partial y_{t-i}$ ,  $b_j$  is equal to  $\partial y_{t+d}/\partial u_{t-j}$ , and that  $c_k$  corresponds to  $\partial y_{t+d}/\partial w_{t+d-k}$ . Since we have an NN forward model of the plant, we can easily calculate the above Jacobians,  $\partial y_{t+d}/\partial y_{t-i}$ ,  $\partial y_{t+d}/\partial u_{t-j}$ , and  $\partial y_{t+d}/\partial w_{t+d-k}$ . This is the basic idea underling

our Jacobian method. The detailed procedure is described below.

### A. Calculation of Jacobians

From Fig. 4, Jacobian is calculated as follows,

$$\begin{aligned}
\frac{\partial y_{t+d}}{\partial x_k} &= \sum_i \frac{\partial y_{t+d}}{\partial O_{2i}} \cdot \frac{\partial O_{2i}}{\partial x_k}, \\
&= \sum_i \{f'(\text{net}_3) \cdot W_i \cdot f'(\text{net}_{2i}) \cdot W_{ik}\}, \\
&= f'(\text{net}_3) \cdot \sum_i W_i \cdot f'(\text{net}_{2i}) \cdot W_{ik}.
\end{aligned} \tag{15}$$

where  $x_k$  stands for any of  $y_t$ ,  $y_{t-1}$ ,  $\dots$ ,  $u_t$ ,  $u_{t-1}$ ,  $\dots$ ,  $w_{t+d}$ ,  $w_{t+d-1}$ ,  $\dots$ , and

$$\text{net}_{2i} = \sum_k O_{1k} \cdot W_{ik}, \quad \text{net}_3 = \sum_i O_{2i} \cdot W_i.$$

### B. Determination of control input

To get a control input that minimizes the cost function (12), we differentiate it with respect to  $u_t$  and put it to zero :

$$\frac{\partial J}{\partial u_t} = (y_{t+d} - d_{t+d}) \frac{\partial y_{t+d}}{\partial u_t} + \rho u_t \tag{16}$$

Since  $\partial y_{t+d}/\partial u_t = b_0$ , substituting Eq.(5)–(8) into  $y_{t+d}$  in Eq.(16) and solving it for  $u_t$ , we get the following control law.

$$\begin{aligned}
u_t &= \left( - \sum_{i=0}^2 a_i y_{t-i} + \sum_{j=1}^d b_j u_{t-j} + \sum_{k=0}^{2d-1} c_k w_{t+d-k} - d_{t+d} \right) \\
&\quad / (b_0 + \rho/b_0)
\end{aligned} \tag{17}$$

If the dead time  $d$  is properly given, then  $b_0$  is non-zero. Coefficient  $\rho$  in the cost function is usually set to be non-negative. Therefore the control law (17) is well defined. Here, the coefficients  $a_i$ ,  $b_j$  and  $c_k$  are given by the Jacobians that are derived from the NN model. The control input  $u_t$  requires values of  $w_{t+d}$ ,  $w_{t+d-1}$ ,  $\dots$ ,  $w_{t+1}$ . Since these are future external signals and thus not available, their predicted values are used instead.

The key point in this paper is to employ control law (17), together with the Jacobian (15), and they are calculated at each time step. Fig. 6 shows the configuration of the Jacobian method. Dotted lines and real lines show off line learning and on line control, respectively.

## 7. Hessian method

We propose the Hessian method to improve the learning speed and to avoid the design parameters to be tuned appropriately depending on the problems. In the cost function (12), let the approximation value of  $u_t$  satisfying  $\partial y_{t+d}/\partial u_t = 0$  to be  $U_t$ , its current

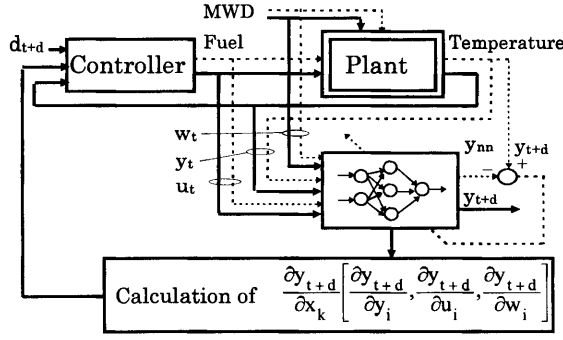


Fig. 6 Configuration of Jacobian method

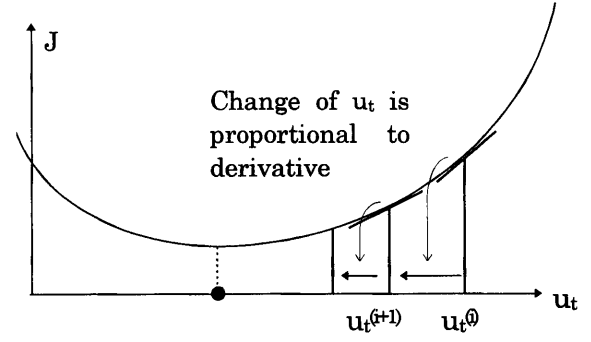


Fig. 7 Iterative inverse method

estimate to be  $U_t^0$  and  $U_t - U_t^0$  to be  $\varepsilon$ .

Expanding  $\frac{\partial J}{\partial u_t} \Big|_{U_t}$  by using Taylor expansion, we get

$$\frac{\partial J}{\partial u_t} \Big|_{U_t} = \frac{\partial J}{\partial u_t} \Big|_{U_t^0} + \varepsilon \cdot \frac{\partial^2 J}{\partial u_t^2} \Big|_{U_t^0}. \quad (18)$$

Putting  $\frac{\partial J}{\partial u_t} \Big|_{U_t} = 0$  gives

$$\varepsilon = - \frac{\frac{\partial J}{\partial u_t} \Big|_{U_t^0}}{\frac{\partial^2 J}{\partial u_t^2} \Big|_{U_t^0}}. \quad (19)$$

Therefore  $u_t$  is given in the following,

$$U_t = U_t^0 + \varepsilon = U_t^0 - \frac{\frac{\partial J}{\partial u_t} \Big|_{U_t^0}}{\frac{\partial^2 J}{\partial u_t^2} \Big|_{U_t^0}}. \quad (20)$$

where

$$\frac{\partial J}{\partial u_t} = (y_{t+d} - d_{t+d}) \cdot \frac{\partial y_{t+d}}{\partial u_t} + \rho \cdot u_t, \quad (21)$$

$$\frac{\partial^2 J}{\partial u_t^2} = \left( \frac{\partial y_{t+d}}{\partial u_t} \right)^2 + (y_{t+d} - d_{t+d}) \cdot \frac{\partial^2 y_{t+d}}{\partial u_t^2} + \rho. \quad (22)$$

Differentiating (14), we have

$$\begin{aligned} \frac{\partial^2 y_{t+d}}{\partial u_t^2} &= f''(\text{net}_3) \cdot \left( \sum_i W_i \cdot f'(\text{net}_{2i}) \cdot (W_{ik})^2 \right. \\ &\quad \left. + f'(\text{net}_3) \cdot \sum_i W_i \cdot f''(\text{net}_{2i}) \cdot W_{ik}^2 \right). \end{aligned} \quad (23)$$

Putting  $f(x) = \frac{1}{1+e^{-x}}$ , its derivatives are given as

$$f' = f \cdot (1-f), \quad f'' = f \cdot (1-f) \cdot (1-2f). \quad (24)$$

So we can obtain the approximate value of  $u_t$  satisfying  $\partial y_{t+d} / \partial u_t = 0$  from (20)–(24) and (14). Though the calculation is somehow complex, we can resolve the drawback of IIM in the on-line control. The  $u_t$  obtained by Eq.(20) is assigned to  $U_t^0$ , and calculation of Eq.(20)–(24) and (14) is repeated, then accuracy of calculation is improved.

Hessian method can be considered from another point of view. Taylor expansion of the cost function in the neighborhood of  $U_t^0$  is expressed by Eq.(25),

$$\begin{aligned} J &= J \Big|_{U_t^0} + (u_t - U_t^0) \cdot \frac{\partial J}{\partial u_t} \Big|_{U_t^0} + \frac{(u_t - U_t^0)^2}{2} \cdot \frac{\partial^2 J}{\partial u_t^2} \Big|_{U_t^0} \\ &\quad + (\text{higher order terms}) \end{aligned} \quad (25)$$

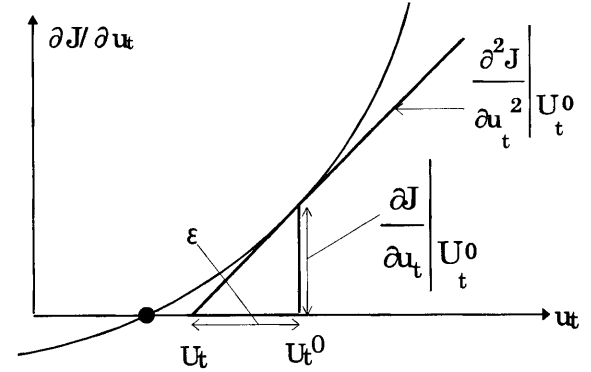


Fig. 8 Hessian method

Taking account of up to second order term of Eq. (25),  $J$  becomes a quadratic function of  $U_t$ . So minimizing  $J$  as the function of  $U_t$ , we can get (20). In other words IIM uses steepest descent method by first order derivative, while Hessian method uses second order derivative of the cost function. This corresponds to the fact that the learning of Gauss-Newton method is much faster than the usual back propagation method in the calculation of weights. It should be noted that weights' calculation time by Gauss-Newton method increases extraordinary with the number of weights. So it is not useful in the case of many weights. On the other hand as for  $u_t$ , it is very useful because only one parameter  $U_t$  is to be calculated. Relation between IIM and Hessian method is shown in Fig. 7 and 8. The  $u_t$  that minimizes the cost function is obtained by IIM iteratively, and in the Hessian method  $u_t$  is calculated that approximates  $\partial y_{t+d} / \partial u_t = 0$  by using second order derivative. Fig. 9 shows the configuration of Hessian method. Dotted lines and real lines show off line learning and on line control, respectively.

## 8. Simulation results

Simulation system consists of a controller model and a power plant model. The power plant model

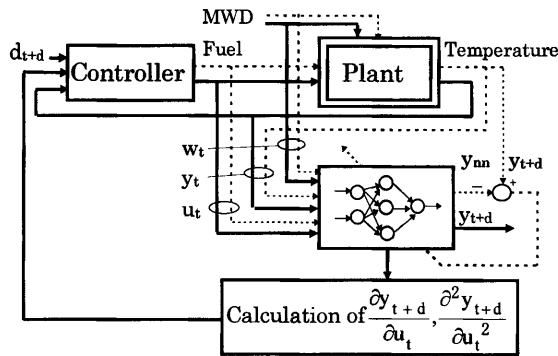


Fig. 9 Configuration of Hessian method

used in the simulations is constituted by the detailed simulator that represents accurately the dynamics of a typical power plant. Fig. 10 shows the simulation flow diagram.

#### A. First step: Acquisition of plant data

Dead time of this plant simulator was about 50 sec., and considering that the sampling interval was 10 sec, we determined  $d=5$ . Fig. 11 shows the training data. In Fig. 11, 0–125% etc. shows the full scale of each variable (the same convention is used in Fig. 12–17). This data shows the time sequence of  $y_t$  (temperature),  $u_t$  (control input) and  $w_t$  (MWD), when the load is changed, for example, 50% → 70% → 100% → 70% → 50% → 100% → 50% at load change rate 2%/min. or 5%/min. The sequential data ( $y_t, \dots, u_t, \dots, w_{t+d}, \dots$ ) to be fed to (9) are obtained from these data.

#### B. Second step: Off line learning

The NN is trained off line by the data of the combination of input ( $y_t, \dots, u_t, \dots, w_{t+d}, \dots$ ) and output  $y_{t+d}$ . Fig. 12 shows training curves which illustrate the learning error (deviation between the desired value and measured value of the NN output) and some of weight values (training iterations: 200000). Error is about 7°C at the beginning of learning (somehow difficult to read it out from the chart), and decreases fast till 1000 iterations, after that decreases gradually, and final error is about 0.3°C and weights converge too.

#### C. Third step: On line control

We studied control performance using Jacobian of NN obtained in the second step and control law (15)–(17). Fig. 13 shows the result of temperature control in the case of load change rate: 2%/min., where only on the coventional PI control (TF=0 in Fig. 1) is used on condition that the load changes 50% → 70% → 100% → 70% → 50%. Temperature deviation is large and becomes larger in the case of 5%/min. load change rate.

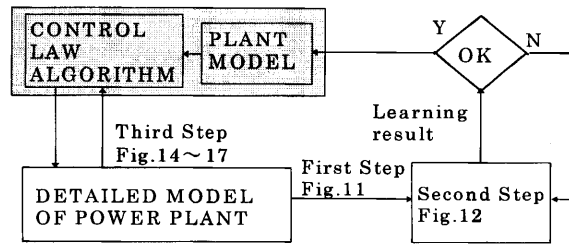
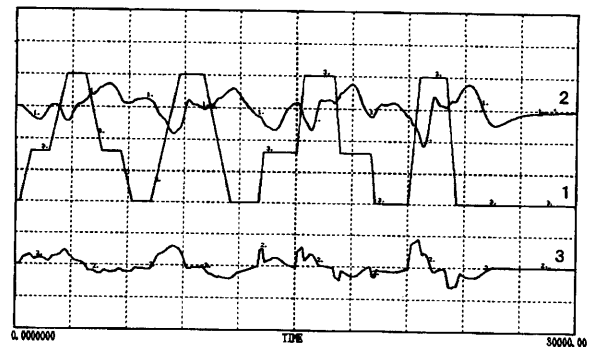
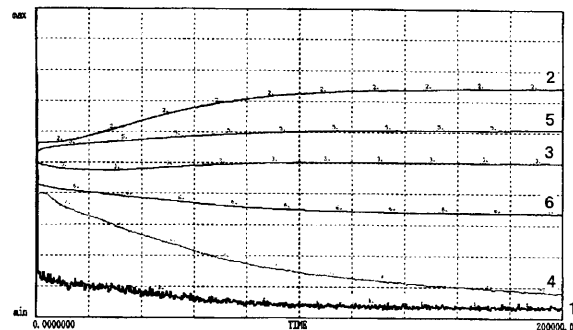


Fig. 10 Simulation flow diagram



1. MWD: 0–125%      2. TEMP.: 400–600°C  
3. DFC: -20–80%      Horizontal axis: 30000sec.

Fig. 11 Examples of Learning Data



1. Deviation: 0–10°C      2. Weight ( $W_{1,1}$ ): -2–2  
3. Weight ( $W_{1,15}$ ): -2–2      4. Weight ( $W_{15,1}$ ): -2–2  
5. Weight ( $W_1$ ): -2–2      6. Weight ( $W_{15}$ ): -2–2  
Horizontal axis: 200000 iterations

Fig. 12 Learning process of NN

The simulation results by IIM are shown in Fig. 14 and 15. Fig. 14 shows the result for the 2%/min. load up/down and NN learning with  $\eta=0.1$  and the number of iteration=5. In this case the control input (fuel) and the plant output (temperature) are not preferable because of their hunting. Fig. 15 shows the result with  $\eta=0.1$  and iteration=100. This case is preferable compared to the case of iteration=5. In IIM there are two parameters i.e., learning rate and the number of iterations, so we have to determine them in



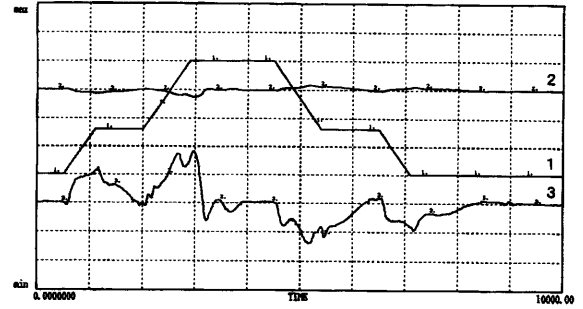
order to get favorable control input. Moreover large  $\eta$  gives hunting in the neighborhood of optimal value, on the other hand small  $\eta$  needs large iterations. Therefore the determination of  $\eta$  is a somehow difficult task.

Fig. 16, 17 show the simulation results derived from Jacobian method, each corresponds to load change rate 2%/min. and free load swing. Control performance is improved very much as is evident from comparison between Fig. 13 and Fig. 16. Hessian method was simulated in the same case and as good performance was obtained as Jacobian method. In the Hessian method, though  $u_i$  was calculated only once, temperature deviation and settling of control input were nearly equal to the case of the Fig. 15.

## 9. Conclusions

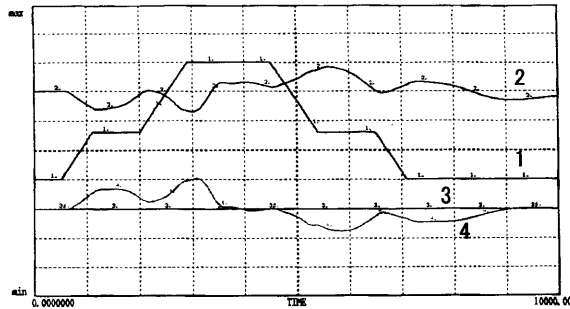
We have already shown that MRAC can not be applied to control the thermal power plant effectively because the persistently exciting conditions is not satisfied<sup>8)</sup>. So, various kinds of neural networks have been studied in order to determine their best architec-

ture and learning algorithm. Especially in this paper, two types of new control laws named Jacobian method and Hessian method are proposed based on the above architecture and learning algorithm. Those methods are advanced versions of iterative inverse method proposed by A. Linden et. al., and the first feature of those methods is the improvement of on line control, and the number of iterative calcula-



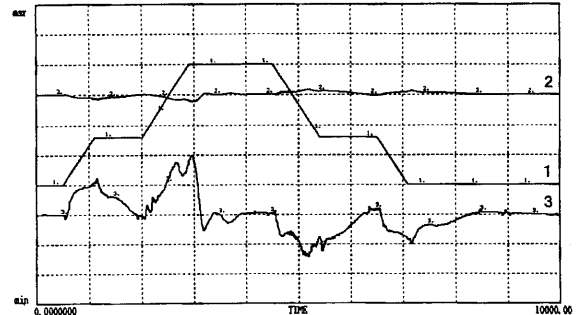
1. MWD: 0-125% 2. TEMP.: 400-600°C  
3. DFC: -12-28 Horizontal axis: 10000sec.

Fig. 15 Load change by IIM (2) (2%/min.)



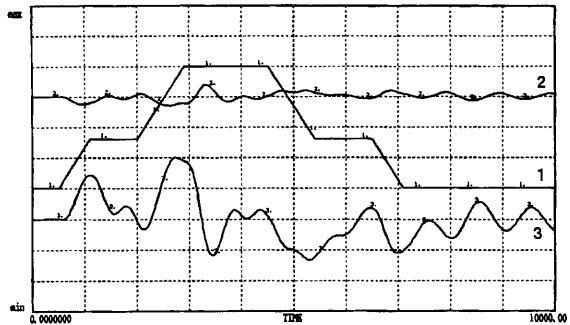
1. MWD: 0-125% 2. TEMP.: 400-600°C  
3. TF: -12-28 4. PI value: -12-28  
Horizontal axis: 10000sec.

Fig. 13 Load change by PI control (2%/min.)



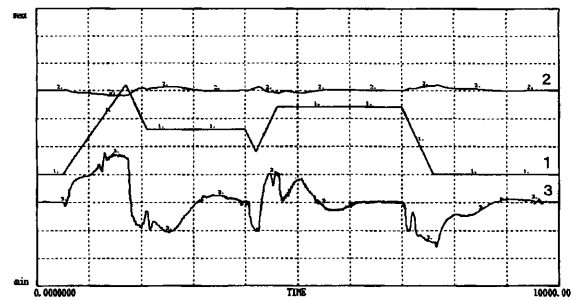
1. MWD: 0-125% 2. TEMP.: 400-600°C  
3. DFC: -12-28 Horizontal axis: 10000sec.

Fig. 16 Load change by Jacobian method (2%/min.)



1. MWD: 0-125% 2. TEMP.: 400-600°C  
3. DFC: -12-28 Horizontal axis: 10000sec.

Fig. 14 Load change by IIM (1) (2%/min.)



1. MWD: 0-125% 2. TEMP.: 400-600°C  
3. DFC: -12-28 Horizontal axis: 10000sec.

Fig. 17 Load change by Jacobian method (free load swing)

tions for finding optimal control law is decreased dramatically. In other words, optimal characteristics of iterative inverse method is obtained in a short computation time using those methods without any adjustment. From the simulation results usefulness and effectiveness of the Jacobian method and Hessian method are proved.

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