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Correlation of Phase Equilibria for Water + Hydrocarbon Systems at High Temperatures and Pressures by Cubic Equation of State

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A modified-Soave-Redlich-Kwong (MSRK) equation of state with an exponent-type mixing rule for the energy parameter and a conventional mixing rule for the size parameter is applied to correlate the phase equilibria for four binary mixtures of water + hydrocarbon (benzene, hexane, decane, and dodecane) systems at high temperatures and pressures. It is noted that good correlation results are obtained by using the mixing rules with interaction parameters between unlike molecules.

Introduction

Recently, many kinds of new chemical processes using supercritical water as a reaction solvent have been studied. The processes, in which waste plastics and biomasses are decomposed rapidly in supercritical water and chemical raw materials are recovered, are the focus of much attention from the stand points of recycling of resources and environmental conservation. In such processes, low molecular weight hydrocarbons such as aromatic compounds and paraffins are produced as decomposed products. Therefore, it is very important to understand phase equilibria for water + hydrocarbon systems at high temperatures and pressures for process design.

Among many methods reported for calculation of phase equilibria, a cubic equation of state seems to be useful because of its simplicity and it can provide successful phase equilibria by selecting suitable mixing rules. The SRK equation of state is one of the most popular cubic equations of state used in process design. In this work, therefore, a modified-SRK (MSRK) equation of state (Sandarusi et al., 1986) was adopted to correlate the phase equilibria. An MSRK equation of state is proposed by modifying the attractive term of the SRK equation of state in order to calculate the saturated vapor pressures of many organic and inorganic compounds accurately. The phase equilibria of four binary mixtures of water + hydrocarbon (benzene, hexane, decane, and dodecane) systems at high temperatures and pressures were correlated by the MSRK equation of state with an exponent-type mixing rule previously proposed (Higashi et al., 1994) for the mixtures containing polar substances.

1. MSRK Equation of State

The MSRK equation of state (Sandarusi et al., 1986) is given as follows.

\[ p = \frac{RT}{(v - b)} - \frac{a(T)}{v(v + b)} \] (1)

where

\[ a(T) = \frac{0.42747\alpha(T)R^2T_c^2}{P_c} \] (2)

\[ b = \frac{0.08664RT_c}{P_c} \] (3)

and

\[ \alpha(T) = 1 + \left(1 - \frac{T_c}{T}\right)\left(m + \frac{n}{T_c}\right) \] (4)

The critical properties required and the parameters \( m \) and \( n \) for water and four hydrocarbons used in the present work are listed in Table 1.
2. Exponent-Type Mixing Rules

In this work, an exponent-type mixing rule proposed in the previous study (Higashi et al., 1994) is adopted for the energy parameter $a$. Namely, the parameter $a$ is given by

$$a = \sum_i \sum_j x_i^{\beta_i} x_j^{\beta_j} a_{ij}$$

(5)

The mixing rule is characterized by the empirical exponent parameters $\beta$ which represent a deviation from random mixing. In this work, the following expressions are assumed for simplicity.

$$\beta_{11} = \beta_{22} = \beta_{21} = 1$$

(6)

Furthermore, the following combining rule is adopted.

$$a_{ij} = \left(1 - k_{ij}\right) \sqrt{a_i a_j}$$

where $k_{ij}$ is the interaction energy parameter between unlike molecules. The following mixing and combining rules are used for the size parameter $b$.

$$b = \sum_i \sum_j x_i x_j b_{ij}$$

(8)

and

$$b_{ij} = \left(1 - l_{ij}\right) \frac{b_i + b_j}{2}$$

(9)

where $l_{ij}$ is the interaction size parameter between unlike molecules. The fugacity required to calculate phase equilibria can be readily derived from Eq. (1) and the mixing rules.

3. Results and Discussion

The phase equilibria for water + decane, + benzene, + dodecane, and + hexane systems, which are typical water + paraffin and water + aromatic compound binary systems, are correlated. The values of $k_{12}$, $l_{12}$, and $\beta_{12}$ are adjusted to give precise fits to the experimental data.

3.1 Water + decane system

Phase equilibria for a water + decane system at 573.2, 593.2, and 613.2 K are correlated. At these temperatures, two different phase equilibrium regions, which are regarded as vapor-liquid equilibria (VLE) and liquid-liquid equilibria (LLE), exist depending on composition and pressure (Wang and Chao, 1990). The authors evaluated the parameters $k_{12}$, $l_{12}$, and $\beta_{12}$. The phase equilibria at the three temperatures can be correlated using the constant parameter values in the LLE region. The values are listed in Table 2. On the other hand, in the VLE region, the parameter $k_{12}$ should be expressed by the following equation;

$$k_{12} = -0.78 + \frac{700}{T}$$

(10)

though $l_{12}$ and $\beta_{12}$ are constants as listed in Table 2.

Figure 1 shows the phase equilibria for the water + decane system. As illustrated in Fig. 1, both VLE and LLE calculated are in good agreement with the experimental data though VLE at 593.2 K show slight deviations. As shown in Table 2, the value of the parameter $\beta_{12}$ is equal to unity for the LLE region, namely, conventional mixing rules give good results in this region. However, contribution of the parameter $\beta_{12}$ is important in the VLE region. In other words, the distribution of molecules in the VLE region seems to be much different from random distribution.

Furthermore, the modified conventional mixing rules which have two adjustable parameters proposed by Adachi and Sugie (1986) are compared with the present mixing rules. The modified conventional mixing rules are shown as follows.

<table>
<thead>
<tr>
<th>Substance</th>
<th>$T_C$ [K]</th>
<th>$p_C$ [MPa]</th>
<th>$m$</th>
<th>$n$</th>
</tr>
</thead>
<tbody>
<tr>
<td>Water</td>
<td>647.3</td>
<td>22.1</td>
<td>0.9500</td>
<td>0.1630</td>
</tr>
<tr>
<td>Benzene</td>
<td>562.1</td>
<td>4.90</td>
<td>0.6043</td>
<td>0.2285</td>
</tr>
<tr>
<td>Hexane</td>
<td>507.4</td>
<td>3.01</td>
<td>0.7446</td>
<td>0.2476</td>
</tr>
<tr>
<td>Decane</td>
<td>617.6</td>
<td>2.11</td>
<td>0.8905</td>
<td>0.3863</td>
</tr>
<tr>
<td>Dodecane</td>
<td>658.2</td>
<td>1.82</td>
<td>0.9604</td>
<td>0.4479</td>
</tr>
</tbody>
</table>

Table 1 Critical properties and parameters $m$ and $n$ (Sandarusi et al., 1986)
where

\[ a = \sum_i \sum_j x_i x_j a_{ij} \]  

(11)

\[ a_{ij} = \left[ 1 - \left( x_i + u_j (x_i - x_j) \right) \right] x_i a_j \]  

(12)

\[ b = \sum_i x_i b_i \]  

(13)

The calculated results are illustrated in Fig. 1. As shown in Fig. 1, it seems difficult to correlate the VLE at 573.2 K by the modified conventional mixing rules proposed by Adachi and Sugie. The present mixing rules can give a particularly good correlation for the VLE in the decane rich phase.

### 3.2 Water + benzene system

In the water + benzene system, correlations are carried out at 498.2, 553.2, 573.2, 579.6, and 603.2 K. In this system, a heteroazeotropic point exists at 498.2 K. Because 553.2 K is above the three-phase critical end point temperature, a heteroazeotropic point does not exist, and the phase diagram consists of both VLE and LLE regions. VLE changes to LLE with increasing pressure. In water rich regions, the vapor phase changes to a liquid phase without a volume change at the transition point. The phase behaviors mentioned above appear from 541.5 to 579.6 K. The critical solution temperature is reported as 579.6 K (Rebert and Kay, 1959).

The values of \( I_{12} \) and \( \beta_{12} \) are determined as constants, and \( k_{12} \) are expressed as a function of temperature as follow.

\[ k_{12} = 0.30 - \frac{49}{T} \]  

(14)

The parameters determined and the correlation performance are listed in Table 2 and illustrated in Fig. 2. In this system, good correlation results are obtained for all temperatures. The vapor phase compositions calculated in the benzene rich phase show slight deviations from the experimental data at 498.2 K.

The performance of the present mixing rules is compared with that of an unsymmetrical mixing rule (Kabadi and Danner, 1985). The unsymmetrical mixing rule was proposed to improve the energy parameter \( a \) for the calculation of water + hydrocarbon systems. As shown in Eq. (15), Kabadi and Danner (1985) divided the water + hydrocarbon interaction term \( a_{w} \) into two terms: \( a'_{w} \) as a measurement of molecule-molecule attraction between water and hydrocarbon and a concentration-dependent term \( a''_{w} \) as a measurement of the structural effect of the hydrocarbon on water. The unsymmetrical mixing rule is shown as follows.
Conclusion

Phase equilibria of four binary systems, namely water + decane, + benzene, + dodecane, and + hexane systems at high temperatures and pressures are correlated by using the MSRK equation of state with an exponent-type mixing rule previously proposed. The calculated results are in good agreement with the experimental data for all systems.

Acknowledgment

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Nomenclature

\begin{align*}
\beta & \text{ exponent in Eq. (5)} \\
\gamma & \text{exponent-type mixing rule}
\end{align*}

\begin{align*}
\text{Literature Cited}
\end{align*}


